

# A highly selective and stable ZnO-ZrO<sub>2</sub> solid solution catalyst for CO<sub>2</sub> hydrogenation to methanol

Jijie Wang, Zelong Li, Chizhou Tang, Zhe Han, Hailong Liu, Zhaochi Feng, Can Li\*

State Key Laboratory of Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, P.R. China

\*Corresponding author: 86-411-84694447, canli@dicp.ac.cn

**Abstract:** A binary metal oxide, ZnO-ZrO<sub>2</sub> solid solution catalyst, which can achieve methanol selectivity up to 86%~91% with CO<sub>2</sub> single-pass conversion over 10% under the similar industrial conditions. The solid solution structure affords dual active site for H<sub>2</sub> activation by Zn site and CO<sub>2</sub> activation by its neighboring Zr site respectively, and is responsible for the excellent catalytic performance.

**Keywords:** CO<sub>2</sub> hydrogenation, methanol synthesis, ZnO-ZrO<sub>2</sub> solid solution.

## 1. Introduction

Methanol synthesis via CO hydrogenation has been industrialized for about 50 years using CuZnOAl<sub>2</sub>O<sub>3</sub> catalyst, which also seems like the best catalyst for methanol synthesis for CO<sub>2</sub> hydrogenation. However, methanol selectivity on CuZnOAl<sub>2</sub>O<sub>3</sub> from CO hydrogenation is near 99%, while that from CO<sub>2</sub> hydrogenation is less than 60% caused by reverse water gas shift reaction (RWGS). The even more severe problem is the rapid deactivation caused by produced water, which accelerates the sintering of Cu active component during the CO<sub>2</sub> hydrogenation. Therefore, new catalyst is needed to develop to realize the process of CO<sub>2</sub> hydrogenation to methanol with high selectivity of methanol.

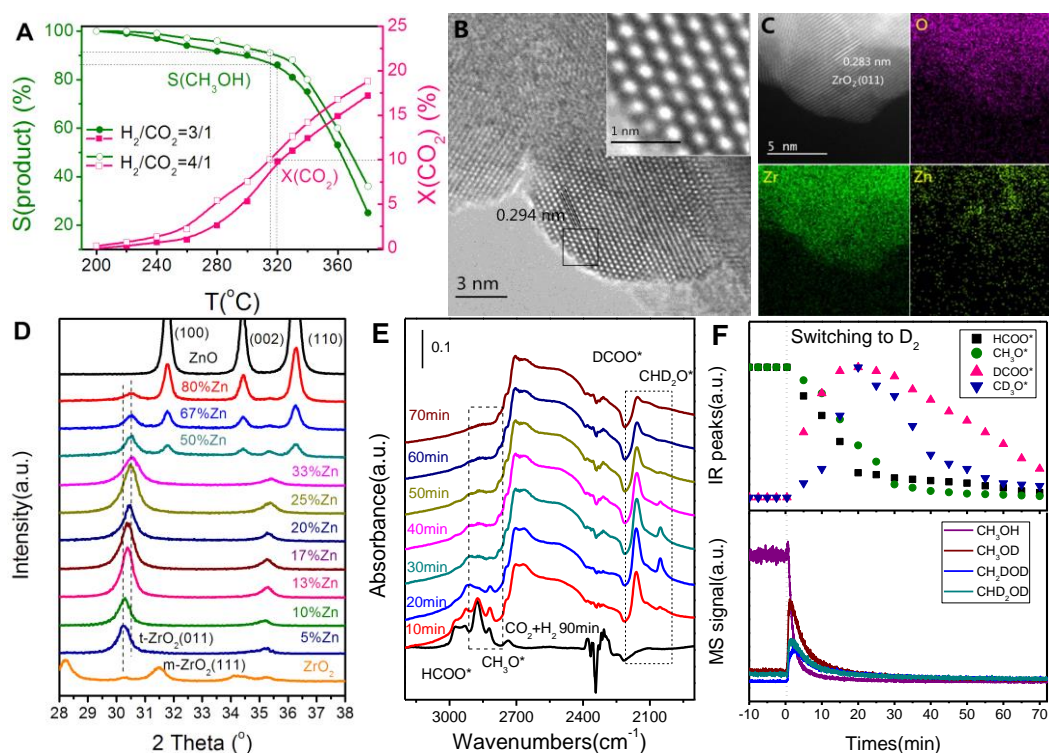
## 2. Experimental

ZnO-ZrO<sub>2</sub> catalyst was synthesized by the co-precipitation method. The activity tests of the catalysts for CO<sub>2</sub> hydrogenation to methanol were carried out in a tubular fixed-bed continuous-flow reactor equipped with gas chromatography (GC). The XRD results were collected on a Philips PW1050/81 diffractometer operating in Bragg-Brentano focusing geometry and using Cu K $\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ) from a generator operating at 40 kV and 30 mA. TEM images were obtained with a JEM-2100 microscope, 200 kV. Element mappings were obtained with a JEM-ARM200F microscope. The CO<sub>2</sub>-TPD of the catalysts was conducted with an adsorption/desorption system and conducted from 50 C to 600 °C. H<sub>2</sub>-D<sub>2</sub> exchange experiments were carried out in a flow reactor at 280 °C. The formation rate of HD was measured by mass signal intensity.

## 3. Results and discussion

ZnO-ZrO<sub>2</sub> solid solution catalyst can achieve methanol selectivity up to 86%~91% with CO<sub>2</sub> single-pass conversion over 10% under the reaction conditions of 5.0 MPa, 24000 mL/(g h), H<sub>2</sub>/CO<sub>2</sub> = 3/1~4/1, 320~315 °C (Fig. 1A). ZnO phase was not observed in XRD when adding ZnO (5–33%) into ZrO<sub>2</sub>, but leads to the phase change of ZrO<sub>2</sub> from monoclinic to tetragonal. The (011) of ZrO<sub>2</sub> shifts to a higher angle when Zn concentration is increased, indicating that ZnO-ZrO<sub>2</sub> is in a solid solution state with Zn incorporated into the ZrO<sub>2</sub> lattice matrix when ZnO contents in the range below 50% (Fig. 1B-D). Their CO<sub>2</sub>-TPD experiments show that most of the CO<sub>2</sub> adsorbed by 13% ZnO-ZrO<sub>2</sub> is on Zr sites, however, H<sub>2</sub>-D<sub>2</sub> experiments suggest that there is a strong synergetic effect in the H<sub>2</sub> activation between the two sites, Zn and Zr. The solid solution structure affords dual active site for H<sub>2</sub> activation by Zn site and CO<sub>2</sub> activation by its neighboring Zr site respectively, and is responsible for the excellent catalytic performance. propose a mechanism of the direct hydrogenation of CO<sub>2</sub> likely via a formate intermediate, rather than consecutive RWGS and CO hydrogenation on ZnO-ZrO<sub>2</sub> solid solution catalyst. HCOO\* and H<sub>3</sub>CO\* species were

observed and identified by *in-situ* diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS). Their further isotopic experiments demonstrate that the surface  $\text{HCOO}^*$  and  $\text{H}_3\text{CO}^*$  species can be hydrogenated to methanol (Fig. 1E-F).



**Figure 1.** (A) The catalytic performance at the reaction temperatures from 200 to 380 °C with  $\text{H}_2/\text{CO}_2 = 3/1$  and  $4/1$ . (B) HRTEM and (C) Aberration-corrected STEM-HAADF images and element distribution of 13%ZnO-ZrO<sub>2</sub>. (D) XRD patterns of ZnO-ZrO<sub>2</sub>. (E) *In-situ* DRIFT spectra of surface species from  $\text{CO}_2 + \text{H}_2$  and subsequently switched to  $\text{D}_2$ . (F) DRIFT-MS of  $\text{CO}_2 + \text{H}_2$  and subsequently switched to  $\text{D}_2$ .

#### 4. Conclusions

ZnO-ZrO<sub>2</sub> binary metal oxide solid solution catalyst was discovered for highly selective and stable hydrogenation of  $\text{CO}_2$  to methanol, which is of interest to both industry and academia. The high selectivity and stability of the ZnO-ZrO<sub>2</sub> catalyst show potential application in carbon capture and utilization (CCU). The dual active sites nature of the solid solution catalyst offers a new opportunity in fine-tuning catalytic activity and selectivity of a wide range of catalysis

#### References

1. G. A. Olah, A. Goepfert, G. K. Surya Prakash, Beyond Oil and Gas: The Methanol Economy (Wiley-VCH, Weinheim, Germany, 2011).
2. J. Graciani, K. Mudiyansele, F. Xu, A. E. Baber, J. Evans, S. D. Senanayake, D. J. Stacchiola, P. Liu, J. Hrbek, J. F. Sanz, J. A. Rodriguez, *Science*, 2014, 345, 546–550.
3. J. J. Wang, G. N. Li, Z. L. Li, C. Z. Tang, Z. C. Feng, H. Y. An, T. F. Liu, H. L. Liu, C. Li, A highly selective and stable ZnO-ZrO<sub>2</sub> solid solution catalyst for  $\text{CO}_2$  hydrogenation to methanol. *Sci. Adv.*, 2017, 3, DOI: 10.1126/sciadv.1701290.