

# Highly Ordered Mesoporous Fe<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> Bimetal Oxides for an Enhanced CO Hydrogenation Activity to Hydrocarbons

**Jae Min Cho,<sup>a</sup> Jong Wook Bae<sup>a,\*</sup>**

<sup>a</sup>*School of Chemical Engineering, Sungkyunkwan University (SKKU), 2066 Seobu-ro, Jangan-gu, Suwon, Gyeonggi-do 16419, Republic of Korea*

*\*Corresponding author: (Tel.) +82-31-290-7347; (Fax.) +82-31-290-7272; (E-mail.) finejw@skku.edu*

**Abstract:** Highly ordered mesoporous Fe<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> mixed bimetal oxides (FeZr) were applied to convert syngas to value-added hydrocarbons through Fischer-Tropsch synthesis reaction. To promote the catalytic activity and structural stability, the irreducible metal oxide of ZrO<sub>2</sub> was incorporated as a structural promoter. At an optimized amount of zirconia (Zr/Fe = 0.25), the activity and structural stability were significantly improved. These enhanced surface properties were mainly due to the formation of the active iron carbide species ( $\gamma$ -Fe<sub>5</sub>C<sub>2</sub>) with insignificant structural collapses by strong interactions between iron nanoparticles and the ZrO<sub>2</sub> structural promoter, which also suppressed the inactive coke depositions.

**Keywords:** ordered mesoporous Fe<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> oxides, structural promoter of ZrO<sub>2</sub>, stable  $\gamma$ -Fe<sub>5</sub>C<sub>2</sub>

## 1. Introduction

Ordered mesoporous metal oxides have been widely utilized in the field of heterogeneous catalysis due to the large size surface area and controllable pore size as well as the enhanced mass transport rate of the products with less catalyst deactivations [1,2]. In order to prevent the catalyst deactivation by the sintering of iron nanoparticles or disintegration of structures during the reaction, ordered mesoporous iron oxide(Fe<sub>2</sub>O<sub>3</sub>) was synthesized by nano-casting method through an incorporation of irreducible ZrO<sub>2</sub> metal oxide as a structural promoter. The ZrO<sub>2</sub> promoter improved the structural stability significantly by forming the strong interactions and facile active iron carbide phases such as  $\gamma$ -Fe<sub>5</sub>C<sub>2</sub> [3].

## 2. Experimental

Irreducible metal oxide ZrO<sub>2</sub> incorporated mesoporous Fe<sub>2</sub>O<sub>3</sub> was synthesized with nano-casting replica method using a hard template of KIT-6 [4,5] at a different molar ratio of Zr/Fe from 0 to 1. The prepared catalysts were denoted as FeZr(x), where x represents the molar ratio of Zr/Fe. Catalytic activity test of the mesoporous FeZr catalysts was carried out in fixed bed reactor at the following reaction conditions: T = 300 °C, P = 2.0 MPa, weight hourly space velocity (WHSV) = 8000 L(mixed gas)/kg<sub>cat</sub>/h and H<sub>2</sub>/N<sub>2</sub>/CO = 63.0/5.5/31.5. Before the FTS reaction, the catalyst was reduced under a flow of 5% H<sub>2</sub>/N<sub>2</sub> at 500 °C for 12 h. The effluent gases from the reactor were analyzed by using an online gas chromatograph (YoungLin 6500 GC) connected with TCD (SUPELCO-12390-U) and FID (HP-PLOT/Q). To characterize the surface properties of FeZr(x), N<sub>2</sub> sorption, TEM, XRD, H<sub>2</sub>-TPR, XPS, XAFS, H<sub>2</sub>-TPSR, Raman spectroscopy, and <sup>57</sup>Fe Mössbauer spectra were carried out.

## 3. Results and discussion

The crystallite size of Fe<sub>2</sub>O<sub>3</sub> was found to be in the range of 11.8 – 32.4 nm. As the amount of ZrO<sub>2</sub> was increased, the smaller Fe<sub>2</sub>O<sub>3</sub> grains were formed due to the well-developed Fe<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> grain structures. However, the X-ray diffraction (XRD) peaks of ZrO<sub>2</sub> were not clearly observed due to its higher dispersion or intrinsic amorphous characters. As the amount of ZrO<sub>2</sub> metal oxide was increased, the specific surface area was also increased from 110.8 to 209.5 m<sup>2</sup>/g due to its structural promoting effect by generating ordered mesoporous structures [6]. The catalytic activities on FeZr(x) are summarized in **Table 1**. Compared with the FeZr(0), the catalytic activities were enhanced in all the ZrO<sub>2</sub> incorporated FeZr catalysts. Among them, FeZr(0.3) showed the most stable catalytic activity with a higher C<sub>5+</sub> and olefin selectivity with the values of 85.6 and 53.6%, respectively. The enhanced FTS activity and stability on the FeZr(0.3) seem to be attributed to an increased degree of reduction and the formation of active and stable iron carbide species instead of a waxy hydrocarbon or coke deposition [7].

**Table 1.** Physicochemical properties and activities of the mesoporous Fe<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> catalysts

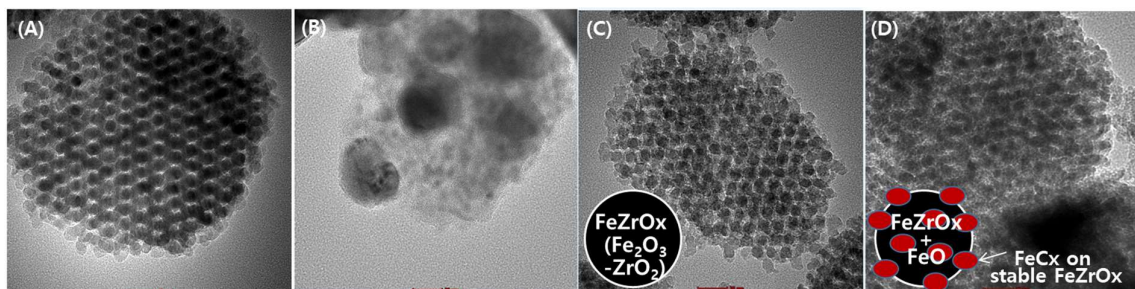
Catalysts	XRD	N <sub>2</sub> sorption	Activity <sup>a</sup>			Product distribution
	Crystallite size of Fe <sub>2</sub> O <sub>3</sub> (nm)	surface area (m <sup>2</sup> /g)	CO conv. (C-mol%)	Olefin sel. (C-mol%) <sup>b</sup>	Chain-growth probability (α) <sup>c</sup>	C <sub>1</sub> / C <sub>2</sub> -C <sub>4</sub> / C <sub>5</sub> +
FeZr(0)	32.4	110.8	5.6	72.4	N.A.	7.6 / 14.1 / 78.3
FeZr(0.1)	22.8	127.9	88.3	42.6	0.917	9.6 / 14.1 / 76.3
FeZr(0.3)	18.8	147.6	82.1	53.6	0.928	4.6 / 9.8 / 85.6
FeZr(0.5)	15.9	147.9	77.0	39.6	0.903	9.9 / 14.1 / 76.0
FeZr(1)	11.8	209.5	44.8	37.5	0.918	9.4 / 13.8 / 76.8

<sup>a</sup>FTS reaction was carried out at the following reaction conditions; T = 300 °C, P = 2.0 MPa, WHSV = 8000 L/kg cat/h, and feed gas composition of H<sub>2</sub>/N<sub>2</sub>/CO = 63.0/5.5/31.5.

<sup>b</sup>Olefin selectivity (C-mol%) was calculated in the C<sub>2</sub> – C<sub>4</sub> light hydrocarbons.

<sup>c</sup>Chain growth probability (α) values were obtained from the Anderson-Schulz-Flory (ASF) distribution in the range of C<sub>12</sub> - C<sub>30</sub> hydrocarbons.

As shown in **Figure 1**, the ZrO<sub>2</sub> incorporated FeZr catalyst preserved the ordered mesoporous structures without any significant structural disintegration after FTS reaction. This structural stability was well related with the suppressed aggregation of active components by stronger interactions with ZrO<sub>2</sub> promoters.



**Figure 1.** TEM image (20nm scale bar) of (A) fresh FeZr(0), (B) used FeZr(0), (C) fresh FeZr(0.3), and (D) used FeZr(0.3).

The structural disintegrations were also clearly verified by XAFS analysis, in which the co-presence of the larger Fe<sub>2</sub>O<sub>3</sub> and metallic Fe phases were observed. In the Mössbauer analysis for the used FeZr catalysts, the content of  $\chi$ -Fe<sub>5</sub>C<sub>2</sub> was found to be higher on the most active FeZr(0.3) due to the stable and smaller iron carbide formation with the help of the strongly interacted FeO-ZrO<sub>2</sub> frameworks.

#### 4. Conclusions

To prevent the structural disintegrations of the mesoporous structures during the reductive FTS reaction conditions, the ordered mesoporous Fe<sub>2</sub>O<sub>3</sub> catalysts were synthesized with an incorporation of the irreducible ZrO<sub>2</sub> oxide via nano-casting technique. The stable and enhanced FTS activity on the FeZr(0.3) seem to be attributed to the stabilized mesoporous structures through the stronger interactions between Fe<sub>2</sub>O<sub>3</sub> and irreducible ZrO<sub>2</sub> crystallites in the main frameworks of FeZr catalysts by facile formation of the well-known active iron carbide phases such as  $\chi$ -Fe<sub>5</sub>C<sub>2</sub> during FTS reaction.

#### References

1. P. Shu, J. Ruan, C. Gao, H. Li, S. Che, *Micropor. Mesopor. Mater.* 123 (2009) 314.
2. J.S. Jung, S.W. Kim, D.J. Moon, *Catal. Today.* 185 (2012) 168.
3. T. Reidel, H. Schulz, G. Schaub, K.W. Jun, K.W. Hwang, K.W. Lee, *Top. Catal.* 26 (2003) 41.
4. S. Sun, X. Zhao, M. Yang, L. Wu, Z. Wen, X. Shen, *Sci. Rep.* 6 (2016) 19564.
5. S. Fei, K. Xia, X. Tian, P. Mei, H. Yan, H. Cheng, *Int. J. Hydrogen Energy.* 41 (2016) 5652.
6. C.I. Ahn, H.M. Koo, J.M. Jo, H.S. Roh, J.B. Lee, Y.J. Lee, E.J. Jang, J.W. Bae, *Appl. Catal. B* 180 (2016) 139.
7. S.H. Kang, J.W. Bae, J.Y. Cheon, Y.J. Lee, K.S. Ha, K.W. Jun, D.H. Lee, B.W. Kim, *Appl. Catal. B* 103 (2011) 169.