

Preparation of metal sulfide catalysts supported on mesoporous and amorphous silica uniformly coated with TiO₂ and ZrO₂

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Abstract: Mesoporous silicas (MSs) and amorphous silicas (ASs) coated with TiO₂ or ZrO₂ layer were used as supports to prepare metal sulfide catalysts for hydrodesulfurization (HDS) of sulfur-containing aromatics. The TiO₂ coating on MSs and ASs of the catalysts increased HDS activity of 4,6-dimethyldibenzothiophene (4,6DMDBT), however, did not by the ZrO₂ coating. This difference in the activity between TiO₂ and ZrO₂ coating was attributed to the enhancement of hydrogenation ability from the correlation with the naphthalene hydrogenation activity of the catalysts.

Keywords: Mesoporous silica, TiO₂ coating, hydrodesulfurization

1. Introduction

Supported metal sulfides have been used as hydrodesulfurization (HDS) catalysts. It is well known that the HDS activities of Mo sulfide catalysts are greatly affected by the support, namely, support effect. However, it is difficult to understand the effects of the support on the catalytic activity because the oxide materials used as supports (Al₂O₃, SiO₂, TiO₂ etc.) are inherently heterogeneous and have different surface areas. Preparation of oxides with high surface is considered a great way to overcome these problems by the coating of surface of amorphous silicas (ASs) or mesopore walls of the mesoporous silicas (MSs) with the oxide layers. Detailed studies of the effects of the support on HDS performance using silica materials coated with oxides are promising for the clarification of support effect of HDS catalysts.

In this study, the TiO₂- and ZrO₂-coated silica materials were applied to catalyst supports for HDS of sulfur-containing aromatics to investigate the support effect of TiO₂- and ZrO₂-supported Mo sulfide catalysts on the catalytic properties for the HDS reaction. Furthermore, we will report the effect of TiO₂- and ZrO₂-coat of the Mo sulfide catalysts on the hydrogenation activity of aromatic compounds.

2. Experimental

CARiACT Q-10 was used as an AS. MSs having mesopores with the diameter of ca. 7 nm was prepared as previously reported¹ using triblock copolymer (Pluronic P-123 EO₂₀PO₇₀EO₂₀), tetraethoxysilane. The TiO₂ and ZrO₂ coating on ASs and MSs was carried out according to the procedure in our previous study¹. The dried MS or AS was dispersed in a dry toluene by sonication. Titanium tetraisopropoxide (Ti/Si = 0.30) or zirconium tetra-n-butoxide in a dry toluene was added dropwisely to the suspension under dry N₂, and the mixture was stirred and washed. The coated silica was dried and calcined to remove the alkoxy groups. This coating procedure was repeated up to 3 times.

Mo oxide catalysts supported on the synthesized mesoporous materials (MoO₃/support) were prepared by a conventional impregnation method using (NH₄)₆Mo₇O₂₄·4H₂O (AHM) as precursor^{1,2}. The catalyst was dried at 100 °C for 16 h and calcined at 500 °C for 5 h. The Mo loading was fixed at 10wt% MoO₃. The MoO₃/support catalyst thus prepared was presulfided at 350 °C for 3 h in a 10% H₂S/H₂ flow at an atmospheric pressure.

The HDS reaction of 4,6-dimethyl-dibenzothiophene (4,6DMDBT) was carried out by batch mode using an autoclave reactor^{1,2}. The sulfided catalyst was suspended in a reactant solution (0.5wt% 4,6-DMDBT solved in tetrahydronaphthalene) in a glove bag filled with N₂. Then suspension was transferred to

an autoclave in the glove bag. The HDS reaction was carried out 330 °C for 4,6-DMDBT. The initial H₂ pressure was 2.0 MPa and the reaction time was 3h. In order to understand the interaction between MoS₂ and the support, naphthalene hydrogenation (HYD) reaction was carried out by the same procedure as above using a reactant solution (1.0wt% naphthalene solved in n-decane) at 300 °C. The reactant and products were analyzed by a gas chromatography equipped with an FID detector. The conversion of DBT and 4,6-DMDBT and naphthalene was calculated from the decreased amount of the reactant.

3. Results and discussion

Table 1 shows the catalytic activities of Mo sulfide catalysts supported on AS and MS for the HDS of 4,6-DMDBT. The Mo/AS without oxide coating did not exhibit the HDS activity. However, Mo/AS coated with TiO₂ three times showed a higher activity, indicating the effectiveness of the TiO₂ coating over AS surface on the HDS activity as with the case of SBA-15 as reported previously¹. Note that the HDS activity of Mo/MS is higher than that of AS for three times TiO₂ coatings, indicating better dispersion of Mo sulfide of Mo/MS due to high surface area. On the other hand, Mo/AS coated with ZrO₂ showed no HDS activity regardless of the number of coating. Mo/AS coated with ZrO₂ one time also showed no HDS activity. These results suggest strong support effect of Mo sulfide catalysts on HDS activity.

In the case of HDS of 4,6-DMDBT, the two methyl groups inhibit the interaction of the sulfur atom with the active site. Therefore, 4,6-DMDBT favors the hydrogenation (HYD) reaction pathway instead of the direct desulfurization (DDS) one because steric hindrance could be avoided³. According to our previous study, it is suggested that hydrogenation activity of catalysts for aromatic compounds is correlated with 4,6-DMDBT HDS activity¹. To clarify the contribution of TiO₂ to reaction pathway for 4,6-DMDBT, reaction naphthalene HYD was carried out for the MS with hybridized coating TiO₂ and ZrO₂. The results were summarized in Table 2. In Table 2, Zr-Zr-Ti represents two times coating with ZrO₂ followed by TiO₂ coating. Table 2 clearly indicates lower HDS and HYD activity of Mo/MS/Ti-Ti-Zr exposing ZrO₂ on the support surface. On the other hand, Mo/MS/Ti-Ti-Zr exposing TiO₂ on the support surface showed higher HDS and HYD activity, indicating acceleration of HDS reaction through HYD pathway for 4,6-DMDBT.

Table 1. HDS activity of Mo sulfide catalysts supported on AS and MS for the HDS of 4,6-DMDBT

catalyst	coat		4,6DMDBT Conversion/%
	oxide	number	
	-	-	0.0
Mo/AS	TiO ₂	1	0.0
		3	8.0
	ZrO ₂	1	0.0
		3	0.0
Mo/MS	-	-	0.94
	TiO ₂	3	21.3
	ZrO ₂	1	0.0

Table 2. Catalytic activities of Mo sulfide catalysts supported on MS with hybridized coating of TiO₂ and ZrO₂ for the HDS of 4,6-DMDBT and HYD of Naphthalene

catatyst	4,6DMDBT Conversion/%	Naphthalene Conversion/%
Mo/MS /Zr-Zr-Ti	8.74	29.9
Mo/MS /Ti-Ti-Zr	0	19.7

4. Conclusions

1. The TiO₂ coating of AS increased the HDS activity for 4,6-DMDBT HDS as well as MS, while The ZrO₂ coating of AS and MS did not show HDS activity for 4,6-DMDBT.
2. The improved HYD ability by TiO₂ coating increase of HDS activity for 4,6-DMDBT but Mo sulfide supported on SiO₂ or ZrO₂-coated surface showed low HYD ability leading to poor HDS activity.

References

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