

NO_x reduction over Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} at low temperature under exhaust gas condition

**Kohei Ueno,^a Takuma Higo,^a Shuhei Ogo,^a Satoshi Hirose,^b Hitoshi Mikami,^b
Yasushi Sekine^{a,*}**

^aDepartment of Applied Chemistry, Waseda University, 3-4-1, Okubo, Shinjuku, Tokyo, 169-8555 Japan

^bHonda R&D, 4630, Shimo-Takanezawa, Tochigi 321-3393 Japan

*Corresponding author: +81-3-5286-3114, ysekine@waseda.jp (Y. Sekine)

Abstract: NO_x reduction by propylene over Ba-substituted LaAlO₃ supported Pd catalyst (Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}) was investigated. Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} revealed higher activity than other Pd catalysts at low temperatures (≤ 573 K) for NO_x reduction by propylene. Comparison with Ba-impregnated LaAlO₃ supported Pd catalyst (Pd/Ba/LaAlO₃) indicated that Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} showed higher activity than Pd/Ba/LaAlO₃. From this result, substitution of La site in the LaAlO₃ support with Ba was more effective for NO_x reduction than Pd/Ba/LaAlO₃ on which Ba was sequentially impregnated.

Keywords: NO_x reduction, Perovskite oxides, Pd catalyst.

1. Introduction

Vehicle exhaust gas contains harmful pollutants such as carbon monoxide (CO), unburned hydrocarbons (HC) and nitrogen oxides (NO_x).¹ Automotive catalysts convert these pollutants into CO₂, N₂ and H₂O.² However, automotive catalysts are faced with problems of lower exhaust gas temperature with improvement of fuel efficiency, less activity of conventional catalysts at low temperature, and severe regulations against automotive emissions. To solve these problems, development of catalysts which show higher activity than conventional catalysts are required. Then, the present study assessed catalytic activity for NO_x reduction by propylene at low temperatures.

2. Experimental

Perovskite-type oxides were prepared using a citric acid complex method. Catalysts were prepared using an impregnation method. The Pd loading amount was 0.5 wt%.

Catalytic activity tests for NO_x reduction were conducted in a fixed bed quartz reactor at atmospheric pressure. Tests were performed with 50 mg of catalyst. The reaction gas composition consisted of 1000 ppm of NO, 500 ppm of C₃H₆, 2000 ppm of O₂, 7 vol% of H₂O, and Ar as a balance gas, simulating the exhaust gas of $\lambda = 1.14$. The total gas flow rate of the reaction gas was 200 cc min⁻¹. Pre-treatment of the catalyst was conducted for oxidation (5 % O₂, Ar balanced at 773 K for 15 min) and reduction (5 % H₂, Ar balanced at 773 K for 15 min). Catalytic activities were measured at 673, 623, 573, 523 and 473 K. NO conversion was analyzed using an online GC-TCD (GC-8A; Shimadzu Corp.). N₂ yield was analyzed using a chemiluminescent method NO_x analyzer (NOA-7000; Shimadzu Corp.).

3. Results and discussion

First, we conducted NO_x reduction by propylene as a model of unburned hydrocarbon in an exhaust gas on Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} and Pd/Al₂O₃ for comparison as a reference catalyst. Catalytic activities on Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} are shown in Fig. 1. Catalytic activities on Pd/Al₂O₃ are shown in Fig. 2. Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} showed higher performance for NO_x reduction reaction than Pd/Al₂O₃ at 473, 523, 573 K. These results suggested that the partial substitution with a different cation (especially Ba) for La site in Pd/LaAlO₃ brought high performance for NO_x reduction reaction.

Alkaline earth metal, particularly Ba, is a component in a lean NO_x trap catalyst (LNT) for NO_x storage. LNT catalysts can convert NO_x to N₂ via nitrate formed by the reaction between surface Ba

species and gaseous NOx under a lean condition, followed by reduction of nitrate to N₂ under a fuel rich condition.

Therefore, to clarify the effect of substitution of La site in the LaAlO₃ support with Ba, we evaluated the catalytic activity of sequentially impregnated Pd/Ba/LaAlO₃ catalyst. Ba loading amount is 6.4wt% which is equal to Ba amount of Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}. Catalytic activities of Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}, Pd/Ba/LaAlO₃ and Pd/LaAlO₃ are presented in Fig.3. Pd/Ba/LaAlO₃ catalyst shows slight increase in NO conversion at 523, 573 K. However, compared to Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}, the catalytic activity of Pd/Ba/LaAlO₃ is inferior to that of Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} at 473 K to 623 K.

According to the above results, La_{0.9}Ba_{0.1}AlO_{3-δ} was found to be superior support of Pd catalyst for NOx reduction. We investigated the role of La_{0.9}Ba_{0.1}AlO_{3-δ} support compared to LaAlO₃, Ba/LaAlO₃ and Al₂O₃ support.

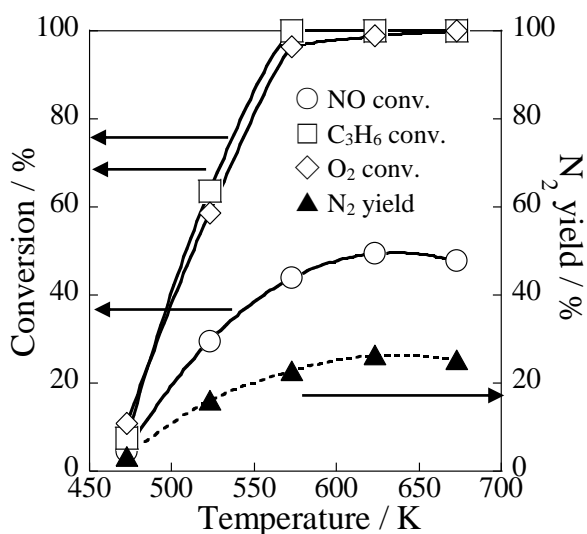


Figure 1. Catalytic activities of Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}.

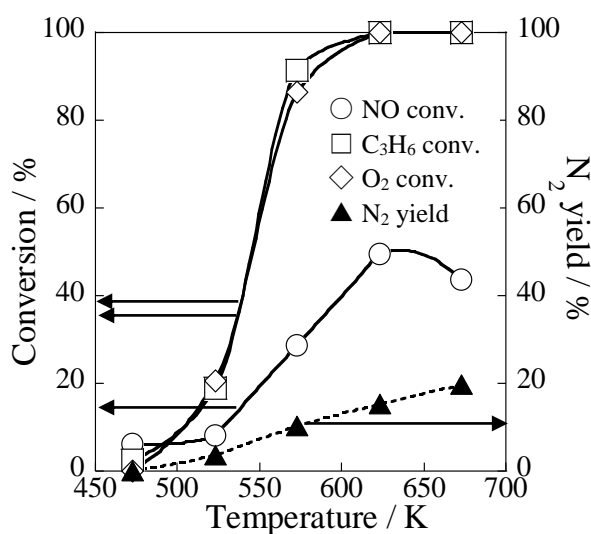


Figure 2. Catalytic activities of Pd/Al₂O₃.

4. Conclusions

We conducted the reduction of NO by C₃H₆ under wet and slightly lean conditions. Pd/La_{0.9}Ba_{0.1}AlO_{3-δ} catalyst showed higher catalytic activity than Pd/Ba/LaAlO₃ and Pd/Al₂O₃ at low temperatures of 523, 573 K. Substitution of La site in LaAlO₃ support with Ba was more effective for NOx reduction.

References

1. A. Fritz, V. Pitchon, *Appl. Catal. B: Environ.* 13 (1997) 1-25.
2. M.V. Twigg, *Appl. Catal. B: Environ.* 70 (2007) 2-15.
3. E. Jobson, *Top. Catal.* 28 (2004) 1-4.

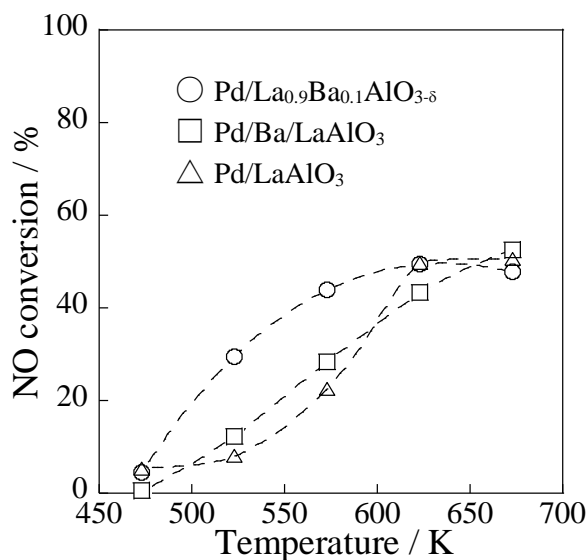


Figure 3. NO conversion of Pd/La_{0.9}Ba_{0.1}AlO_{3-δ}, Pd/Ba/LaAlO₃ and Pd/LaAlO₃.