

TS-1 Supported Precious Metal Catalysts for the Direct Synthesis of Hydrogen Peroxide

Richard J. Lewis^{a*}, Kenji Ueura^b, Yukimasa Fukuta^b, Jennifer. K. Edwards^a, David J. Morgan^a, Simon J. Freakley^a, Christopher J. Kiely^{a,c}, Yasushi Yamamoto^b Graham J. Hutchings^{a*}

^aCardiff Catalysis Institute, School of Chemistry, Cardiff University, Main Building, Park Place, Cardiff, CF10 3AT, UK.

^bUBE Industries, 1978-5, Kogushi, Ube, Yamaguchi 755-8633, Japan

^c Department of Materials Science and Engineering, Lehigh University, 5 East Packer Avenue, Bethlehem, Pennsylvania, PA 18015, USA.

*lewisr27@cardiff.ac.uk, Hutch@cardiff.ac.uk

Abstract:

We demonstrate high catalytic activity towards hydrogen peroxide (H₂O₂) generated from molecular H₂ and O₂ using Au-Pd-Pt trimetallic catalysts supported on a commercial titanium silicate (TS-1). H₂O₂ generation via the direct combination of H₂ and O₂ presents an attractive and atom efficient route to an important commodity chemical removing the financial and environmental drawbacks associated with the Anthraquinone Oxidation (AO) process, the current industrial process for H₂O₂ synthesis.

Keywords: Hydrogen Peroxide, Gold-Palladium, Direct Synthesis

1. Introduction

Hydrogen peroxide is an important commodity chemical, used primarily as a bleaching agent or disinfectant. In addition the high oxygen content and ‘green’ credentials of H₂O₂ has accounted for an increasing interest in its use as an oxidant for chemical synthesis. Titanium silicate-1 (TS-1) has widely been reported to offer high selectivity and efficiency in oxidation reactions alongside pre-formed H₂O₂, with the catalytic conversion of propylene to propylene oxide a key industrial process¹. A significant cost to this process is incurred from the production, concentration, transportation and dilution of H₂O₂, which can be overcome via producing H₂O₂ at source. In this contribution we show that the H₂O₂ can be produced by supporting trimetallic nanoparticles on the titanium silicate to form a composite catalyst for H₂O₂ generation.

2. Experimental

Catalyst Preparation.

0.66 wt. % Au-Pd and Au-Pd-Pt catalysts supported on a commercial TS-1 have been prepared by a wet impregnation procedure that is scalable to industrial requirements, using PdCl₂, H₂PtCl₆ and HAuCl₄.3H₂O as metal precursors. Catalysts were dried and ground prior to calcination in static air, to produce stable and reusable catalysts.

Direct synthesis of H₂O₂.

Hydrogen peroxide synthesis was evaluated using a Parr Instruments stainless steel autoclave with a nominal volume of 100 ml and a maximum working pressure of 14 MPa. To test each catalyst for H₂O₂ synthesis, the autoclave was charged with catalyst, solvent (MeOH and H₂O). The autoclave was with 5% H₂/CO₂, followed by the addition of 25 % O₂/CO₂ to give a hydrogen to oxygen ratio of 1 : 2 and a total pressure of 4.0 MPa. The temperature was then decreased to 2 °C followed by stirring

of the reaction mixture for 30 min. H_2O_2 productivity was determined by titrating aliquots of the final solution after reaction with acidified $\text{Ce}(\text{SO}_4)_2$ (0.01 M) in the presence of ferroin indicator.

3. Results and discussion

Low loaded Au-Pd catalysts supported on a commercial TS-1 are shown to offer high yields of cyclohexanone oxime, via the in-situ synthesis of H_2O_2 from molecular H_2 and O_2 . A small addition of Pd to monometallic Au resulted in a significant increase H_2O_2 synthesis activity, as seen previously when these catalysts have been prepared on common oxide supports.

With the addition of a small amount of Pt catalyst selectivity towards H_2O_2 , under our standard reaction conditions, improves and an enhancement in the rate of H_2O_2 synthesis is seen, from 44 to 56 $\text{mol}_{\text{H}_2\text{O}_2} \text{kg}_{\text{cat}}^{-1} \text{h}^{-1}$. With this value comparable to that observed for the well studied 5 % AuPd / TiO_2 catalyst², despite much lower metal loadings. We ascribe the increase in catalytic activity with Pt addition to an increase in the Pd : Au surface ratio, as derived from XPS analysis. We report an increase in the Pd : Au surface ratio upon incorporation of 0.11 wt. % Pt, with a similar enhancement reported previously for Au-Pd catalysts supported on CeO_2 ³ and TiO_2 ⁴. This effect can be attributed to the enhancement of the core-shell morphology via the addition of Pt or by a higher dispersion of Pd rich particles on the surface of the TS-1 support.

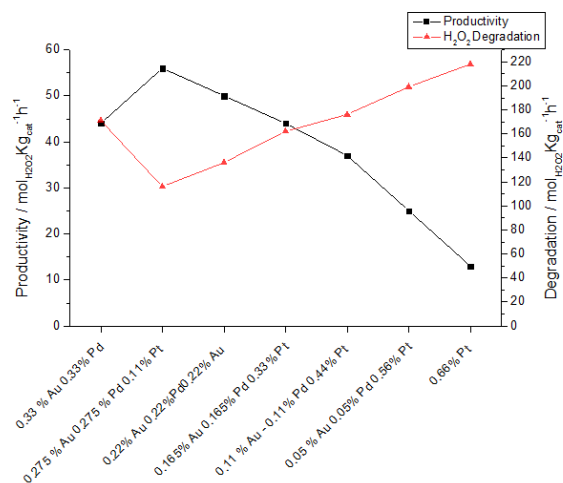


Figure 1. The effect of Pt addition to AuPd / TS-1 on catalytic activity towards H_2O_2 synthesis and its subsequent degradation.

4. Conclusions

We have demonstrated that it is possible to achieve significantly high yields of H_2O_2 , a key commodity chemical for a range of chemical syntheses. The talk will focus on the relationship between catalyst composition and activity towards the direct synthesis of H_2O_2 , with particular interest in the potential application of in-situ generated H_2O_2 as an oxidising agent when used alongside TS-1.

References

1. M.G. Clerici, G. Bellussi, U. Romano, *J. Catal.*, 1991, **129**, 159-167
2. J. K. Edwards, B. E. Solsona, P. Landon, A. F. Carley, A.A. Herzing, C.J. Kiely, and G. J. Hutchings., *J. Catal.*, 2005, **236**, 69-79.
3. J. K. Edwards, J. Pritchard, L. Lu, M. Piccinini, G. Shaw, A. F. Carley, D.J. Morgan, C.J. Kiely, and G. J. Hutchings, *Angew. Chem. Int. Ed.*, 2014, **53**, 2381–2384
4. J. K. Edwards, J. Pritchard, P. J. Miedziak, M. Piccinini, A. F. Carley, Q. He, C. J. Kiely and G. J. Hutchings, *Catalysis Science & Technology*, 2014, **4**, 3244-3250